

Gas-phase Hydroformylation of 1-Butene using Monolithic Supported Liquid-Phase (SLP) Catalyst

<u>Mahtab Madani¹</u>, Leonhard Schill¹, Nanette Zahrtmann², Raquel Portela³, Linda Arsenjuk⁴, Robert Franke⁴, Rasmus Fehrmann¹, Anders Riisager¹

¹Centre for Catalysis and Sustainable Chemistry, Department of Chemistry, Technical, University of Denmark, Lyngby, Denmark ²LiqTech Ceramics A/S, Ballerup, Denmark, ³Institute of Catalysis and Petrochemistry (ICP-CSIC), Spectroscopy and Industrial Catalysis Group. Madrid, Spain, ⁴Evonik Operations GmbH, Marl, Germany









- MACBETH project
- Hydroformylation (HyFo) of olefins
- SLP system
- SLP HyFo catalytic testing
- Summary & outlook



MACBETH project







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Acronym:

Membrane And Catalysts Beyond Economic and Technological Hurdles

Goals:

- Development of new supported liquid-phase catalysts
- Reactor systems development for large-scale chemicals production

Impacts:

- Reduction of GHGs
- Increase of resources & energy efficiency
- Reduce operational & investment costs









- 24 partners
- 10 countries
- 6 plant/testing sites (?)





🖄 macbeth.h2020@gmail.com





MACBETH cases

HyFo - Hydroformylation

Conversion of olefins & syngas to aldehydes

Production of specialty chemicals



H₂ – Hydrogen Production

Natural gas methane conversion to hydrogen





PDH – Propane Dehydrogenation

Conversion of propane to propylene

Production of petrochemicals



BOC – Bio Catalytical Oil Cleavage

Conversion of vegetable oils to fatty acids or their alkyl ester derivates

Food industry and biofuels





Hydroformylation of olefins









Hydroformylation (HyFo) reaction



- > 10 mio. t per year
- Homogeneously catalyzed process
- Huge incentive for heterogenization



Chem. Rev. 2012, 112, 11, 5675



Supported Liquid-Phase (SLP) System

A bridge between heterogeneous & homogeneous catalysis









Catalysis classifications

Heterogeneous Catalysis

Advantages:

- Straightforward catalyst/product separation
- Simple reactor design

Drawbacks:

- Low selectivity
- Low mechanistic understanding

Homogeneous Catalysis

Advantages:

- High selectivity
- High activity
- Deep mechanistic understanding

Drawbacks:

Difficult catalyst/product separation

Heterogenized homogeneous Catalysis

- Secure the advantages of both homogeneous & heterogeneous catalysis
- An example \rightarrow SLP system





SLP system

- SLP system \rightarrow one example of heterogenized homogeneous catalysis
- Immobilization of a homogeneous catalyst solution on a solid support
- Secure the advantages of both homogeneous & heterogeneous catalysis







Monolithic SiC support

Monolithic SiC support:

- Chemically inert
- Efficient thermal conductivity
- Reduced pressure drop
- Simple up-scaling by modular design









Monolithic SiC support – leaching issue

Large macropores in the SiC monolith

Too weak capillary forces

Catalyst system leaching

New porous monoliths have to be developed

Infiltration by metal oxide (SiO₂) nanoparticles



Portela et al., Reaction Chemistry & Engineering, 2021, 6, 2114







Monolithic support structure









Macropores (~ 10 µm)

Si

 SiO_2 washcoat

- Mesopores (~ 3-30 nm)
- Provides high surface area
- Better liquid catalyst dispersion
- Smooth surface for membrane application

J. M. Marinkovic, Technical University of Denmark, 2019



SiC skin



Support variations

Variable parameters:

Number of SiO₂ washcoat layers

• Size of the SiO₂ washcoat particles

Support name	SiO2 particle size (nm)	# of washcoat layer	Intermediate washcoat calcination	Theo. Size of mesopores (nm)
1×Si 7	7	1	-	2.8
1×Si 70	70	1	-	28
2×Si 70	70	2	-	28
2×Si 70-calc.	70	2	✓	28

Portela et al., Catalysis Today. 2022, 383, p 44-54





Support structure

SEM on SiC monolith





Mercury Intrusion porosimetry (MIP)

Silica NPs infiltration shows trimodal pore size distribution comprising meso, small & large macropores

16

J. M. Marinkovic, Technical University of Denmark, 2019





SLP catalyst system

Impregnation of a porous solid material with the homogeneous catalyst solution

Monolithic support



Catalyst stock solution

SLP catalyst



Sebacate melts at the reaction temperature & forms the liquid-phase





The overall SLP system





SLP HyFo catalytic testing

Monolithic supported Rh-catalysts in gas-phase HyFo of 1-butene









SLP HyFo-rig and reaction conditions

Aim:

Structure-catalytic performance correlation in different supports

- T = 120 °C
- $P_{feed} = 10 \text{ bar}$
- Rh/bpp/sebacate molar ratio = 1/4/16
- Rh loading = ca. 0.01 wt.%
- TOS = 0-44 h \rightarrow start-up conditions
- TOS = 44-140 h → standard conditions (syngas = 4.46, 1-butene = 1.045, N₂ = 5.67 mmol.min⁻¹)







Catalytic performance results

Catalyst selectivity

- Higher aldol accumulation in 7 nm SiO₂ washcoat containing support due to smaller pore size in the washcoat (2.8 vs. 28 nm)
- Steady decrease of n/iso-aldehyde due to autocatalytic decomposition of bpp ligand









Catalytic performance results

Catalyst activity

 Steady decrease of 1-butene conversion in 7 nm SiO₂ washcoat containing support → due to higher aldol formation









Summary & outlook

- Silica washcoated monolithic SiC supports with different porosity were developed for 1-butene HyFo after impregnation with a homogeneous Rh-catalyst system
- Catalytic performance showed better catalytic activity for 70 nm silica washcoated supports along with desired negligible aldol formation
- Better *n*-pentanal selectivity in 7 nm silica washcoated support
- Prominent catalytic performance in different support modifications and long-term stability
- Outlook → optimization of catalyst components → e.g. optimization of the ratio between active catalyst components, liquid loading, etc.



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